

6.118 For the piping system of Fig. P6.118, all pipes are concrete with a roughness of 0.04 inch. Neglecting minor losses, compute the overall pressure drop $p_1 - p_2$ in lbf/in^2 . The flow rate is $20 \text{ ft}^3/\text{s}$ of water at 20°C .

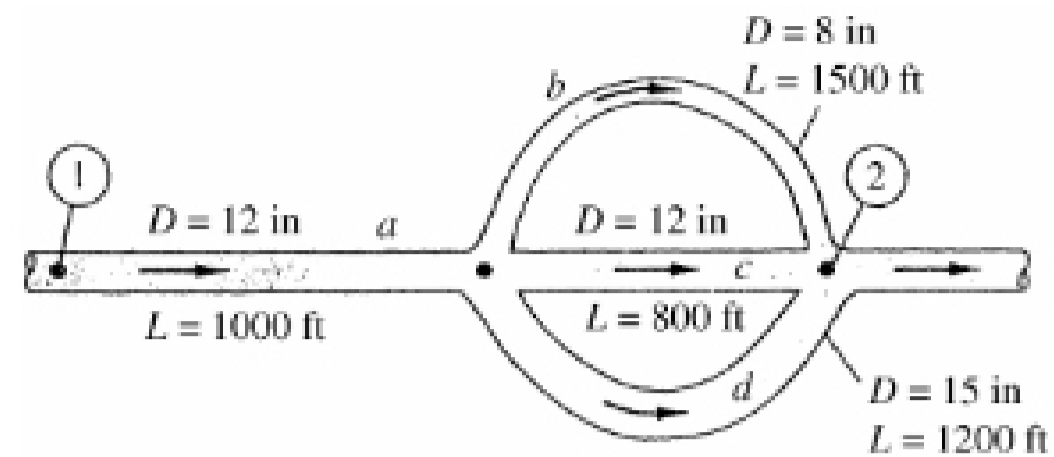


Fig. P6.118

Solution: For water at 20°C , take $\rho = 1.94 \text{ slug/ft}^3$ and $\mu = 2.09\text{E-}5 \text{ slug/ft}\cdot\text{s}$. Since the pipes are all different make a little table of their respective L/d and ε/d :

(a)	$L = 1000 \text{ ft}$,	$d = 12 \text{ in}$,	$L/d = 1000$,	$\varepsilon/d = \mathbf{0.00333}$
(b)	1500 ft	8 in	2250	$\mathbf{0.00500}$
(c)	800 ft	12 in	800	$\mathbf{0.00333}$
(d)	1200 ft	15 in	960	$\mathbf{0.00267}$

With the flow rate known, we can find everything in pipe (a):

$$V_a = \frac{Q_a}{A_a} = \frac{20}{(\pi/4)(1 \text{ ft})^2} = 25.5 \frac{\text{ft}}{\text{s}}, \quad \text{Re}_a = \frac{1.94(25.5)(1)}{2.09\text{E-}5} = 2.36\text{E}6, \quad f_a \approx 0.0270$$

Then pipes (b,c,d) are in parallel, each having the same head loss and with flow rates which must add up to the total of $20 \text{ ft}^3/\text{s}$:

$$h_{fb} = \frac{8f_b L_b Q_b^2}{\pi^2 g d_b^5} = h_{fc} = \frac{8f_c L_c Q_c^2}{\pi^2 g d_c^5} = h_{fd} = \frac{8f_d L_d Q_d^2}{\pi^2 g d_d^5}, \quad \text{and} \quad Q_b + Q_c + Q_d = 20 \frac{\text{ft}^3}{\text{s}}$$

Introduce L_b, d_b , etc. to find that $Q_c = 3.77Q_b(f_b/f_c)^{1/2}$ and $Q_d = 5.38Q_b(f_b/f_d)^{1/2}$

Then the flow rates are iterated from the relation

$$\Sigma Q = 20 \frac{\text{ft}^3}{\text{s}} = Q_b [1 + 3.77(f_b/f_c)^{1/2} + 5.38(f_b/f_d)^{1/2}]$$

$$\text{First guess: } f_b = f_c = f_d: \quad Q_b \approx 1.97 \text{ ft}^3/\text{s}; \quad Q_c \approx 7.43 \text{ ft}^3/\text{s}; \quad Q_d \approx 10.6 \text{ ft}^3/\text{s}$$

Improve by computing $\text{Re}_b \approx 349000$, $f_b \approx 0.0306$, $\text{Re}_c \approx 878000$, $f_c \approx 0.0271$, $\text{Re}_d \approx 1002000$, $f_d \approx 0.0255$. Repeat to find $Q_b \approx 1.835 \text{ ft}^3/\text{s}$, $Q_c \approx 7.351 \text{ ft}^3/\text{s}$, $Q_d \approx 10.814 \text{ ft}^3/\text{s}$. Repeat once more and quit: $Q_b \approx 1.833 \text{ ft}^3/\text{s}$, $Q_c \approx 7.349 \text{ ft}^3/\text{s}$, $Q_d \approx 10.819 \text{ ft}^3/\text{s}$, from which $V_b \approx 5.25 \text{ ft/s}$, $V_c \approx 9.36 \text{ ft/s}$, $V_d \approx 8.82 \text{ ft/s}$. The pressure drop is

$$\begin{aligned} p_1 - p_2 &= \Delta p_a + \Delta p_b = f_a \frac{L_a}{d_a} \frac{\rho V_a^2}{2} + f_b \frac{L_b}{d_b} \frac{\rho V_b^2}{2} \\ &= 17000 + 1800 \approx 18800 \text{ psf} \approx \mathbf{131 \frac{\text{lbf}}{\text{in}^2}} \quad \text{Ans.} \end{aligned}$$

6.130 In Fig. P6.130 lengths AB and BD are 2000 and 1500 ft, respectively. The friction factor is 0.022 everywhere, and $p_A = 90 \text{ lbf/in}^2$ gage. All pipes have a diameter of 6 in. For water at 20°C , determine the flow rate in all pipes and the pressures at points B , C , and D .

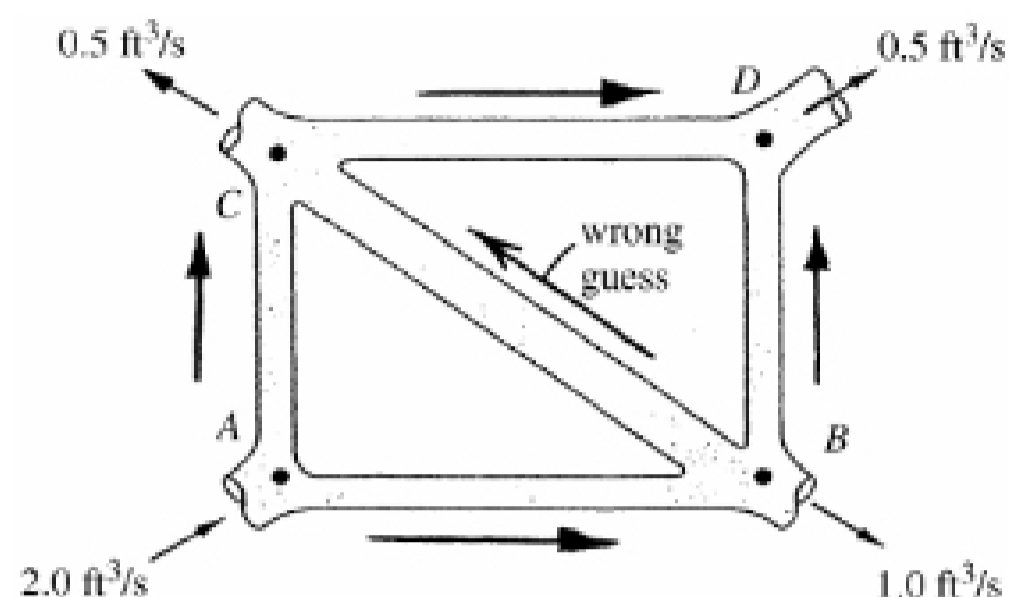


Fig. P6.130

Solution: For water at 20°C , take $\rho = 1.94 \text{ slug/ft}^3$ and $\mu = 2.09\text{E}-5 \text{ slug/ft}\cdot\text{s}$. Each pipe has a head loss which is known except for the square of the flow rate:

$$\text{Pipe AC: } h_f = \frac{8fLQ^2}{\pi^2gd^5} = \frac{8(0.022)(1500)Q_{AC}^2}{\pi^2(32.2)(6/12)^5} = K_{AC}Q_{AC}^2, \quad \text{where } K_{AC} \approx 26.58$$

Similarly, $K_{AB} = K_{CD} = 35.44$, $K_{BD} = 26.58$, and $K_{BC} = 44.30$.

$$\text{Loop ABC: } 35.44Q_{AB}^2 + 44.3Q_{BC}^2 - 26.58Q_{AC}^2 = 0$$

$$\text{Loop BCD: } 44.3Q_{BC}^2 + 35.44Q_{CD}^2 - 26.58Q_{BD}^2 = 0$$

$$\text{Junctions A,B,C: } Q_{AB} + Q_{AC} = 2.0;$$

$$Q_{AB} = Q_{BC} + Q_{BD} + 1.0; \quad Q_{AC} + Q_{BC} = Q_{CD} + 0.5$$

After solving the above equations:

$$Q_{AB} = 0.949 \text{ ft}^3/\text{s} \text{ (toward B); } \quad Q_{AC} = 1.051 \text{ ft}^3/\text{s} \text{ (toward C)}$$

$$Q_{BC} = 0.239 \text{ (toward B); } \quad Q_{CD} = 0.312 \text{ (toward D); } \quad Q_{BD} = 0.188 \text{ (to D)} \quad \text{Ans. (a)}$$

The pressures start at A, from which we subtract the friction losses in each pipe:

$$p_B = p_A - \rho g K_{AB} Q_{AB}^2 = 90 \times 144 - 62.4(35.44)(0.949)^2 = 10969 \text{ psf} \div 144 = 76 \text{ psi}$$

$$\text{Similarly, we obtain } p_C = 11127 \text{ psf} = 77 \text{ psi; } \quad p_D = 10911 \text{ psf} \approx 76 \text{ psi} \quad \text{Ans. (b)}$$